

# BIO ROUTES TO *PARA*-XYLENE

## Table of Contents

A Report by Nexant's CHEMSYSTEMS  
Process Evaluation/Research Planning (PERP) Program  
PERP 2011S3 - Published March 2012

[www.chemsystems.com](http://www.chemsystems.com)

Section	Page
<b>1 Executive Summary</b> .....	1
1.1 INTRODUCTION .....	1
1.2 RENEWABLE ROUTES TO <i>PARA</i> -XYLENE.....	2
1.2.1 Dimerization .....	3
1.2.2 Dehydrocyclization .....	4
1.3 COMPANIES DOING RESEARCH FOR PRODUCING BIO <i>PARA</i> -XYLENE .....	4
1.3.1 Anellotech, Inc. ....	4
1.3.2 Gevo, Inc. ....	5
1.3.3 Global Bioenergies.....	5
1.3.4 Pacific Northwest National Laboratory (PNNL) and Washington State University (WSU).....	6
1.3.5 UOP.....	7
1.3.6 Virent Energy Systems, Inc. ....	7
1.4 COMMERCIAL TECHNOLOGY .....	7
1.5 ECONOMIC ANALYSIS .....	10
1.6 COMMERCIAL ANALYSIS.....	10
1.6.1 Global.....	10
1.6.2 United States .....	11
1.6.3 Western Europe.....	12
1.6.4 Asia Pacific .....	13
1.7 CONCLUSIONS.....	14
<b>2 Bio Technology</b> .....	16

2.1	INTRODUCTION .....	16
2.2	RENEWABLE ROUTES TO <i>PARA</i> -XYLENE.....	17
2.2.1	Dimerization .....	18
2.2.2	Dehydrocyclization.....	24
2.3	COMPANIES DOING RESEARCH FOR PRODUCING BIO <i>PARA</i> -XYLENE .....	28
2.3.1	Anellotech, Inc. ....	28
2.3.2	Gevo, Inc. ....	33
2.3.3	Global Bioenergies.....	42
2.3.4	Pacific Northwest National Laboratory (PNNL) and Washington State University (WSU).....	43
2.3.5	UOP.....	43
2.3.6	Virent Energy Systems, Inc. ....	48
<b>3</b>	<b>Commercial Technology</b> .....	<b>55</b>
3.1	INTRODUCTION .....	55
3.2	XYLENES PRODUCTION.....	57
3.2.1	Catalytic Reforming.....	58
3.2.2	Pyrolysis Gasoline .....	62
3.2.3	Toluene Disproportionation (TDP), Transalkylation, and Dealkylation.....	64
3.3	XYLENES RECOVERY .....	75
3.3.1	Introduction.....	75
3.3.2	<i>para</i> -Xylene .....	78
3.3.3	Isomerization.....	102
3.4	SPECIFICATION .....	105
<b>4</b>	<b>Economic Analysis</b> .....	<b>106</b>
4.2	PROCESS ECONOMICS.....	109
4.2.1	Cost of Production .....	109
4.2.2	Sensitivities .....	121
4.3	CONCLUSIONS.....	127
<b>5</b>	<b>Commercial Analysis</b> .....	<b>129</b>
5.1	APPLICATIONS OF <i>PARA</i> -XYLENE.....	129
5.2	GLOBAL .....	130
5.2.1	Consumption.....	130
5.2.2	Supply .....	131

5.2.3	Supply, Demand, and Trade.....	132
5.3	UNITED STATES .....	134
5.3.1	Consumption .....	134
5.3.2	Supply .....	134
5.3.3	Supply, Demand, and Trade.....	136
5.4	WESTERN EUROPE .....	137
5.4.1	Consumption .....	137
5.4.2	Supply .....	138
5.4.3	Supply, Demand, and Trade.....	139
5.5	ASIA PACIFIC .....	141
5.5.1	Consumption .....	141
5.5.2	Supply .....	142
5.5.3	Supply, Demand, and Trade.....	147
<b>6</b>	<b>References</b> .....	<b>149</b>

		Page
<b>Appendix</b>		
<b>A</b>	<b>List of Acronyms and Abbreviations</b> .....	A-1
<b>B</b>	<b>Definitions of Capital Cost Terms Used in Process Economics</b> .....	B-1
<b>C</b>	<b>Definitions of Operating Cost Terms Used in Process Economics</b> .....	C-1
<b>D</b>	<b>PERP Program Title Index (2001/2002 - 2011)</b> .....	D-1

Figure	Page
1.1 How to Make 100 Percent Renewable PET.....	2
1.2 Process Options for Producing <i>para</i> -Xylene from Isobutylene.....	3
1.3 Mixed Xylene Technology .....	8
1.4 <i>para</i> -Xylene Cost of Production.....	10
1.5 Global <i>para</i> -Xylene Net Trade .....	11
1.6 United States <i>para</i> -Xylene Supply, Demand, and Trade.....	12
1.7 Western Europe <i>para</i> -Xylene Supply, Demand, and Trade .....	13
1.8 Asia Pacific <i>para</i> -Xylene Supply, Demand, and Trade.....	14
1.9 Renewable versus Conventional Routes to PX.....	15
2.1 How to Make 100 Percent Renewable PET* .....	17
2.2 Process Options for Producing <i>para</i> -Xylene from Isobutylene.....	18
2.3 Simplified Block Flow Diagram for Anellotech’s Biomass to Aromatics™ Process.....	29
2.4 Proposed Reaction Scheme for Catalytic Fast Pyrolysis .....	31
2.5 Gevo’s Block Flow Diagram for Isobutylene Production .....	34
2.6 Gevo’s Pathway to Isobutanol .....	35
2.7 Simple Flow Diagram for U.S. Patent Application 2011/0087000 .....	36
2.8 Integrated System to Convert Isobutanol to Renewable <i>para</i> -Xylene .....	38
2.9 UOP Block Flow Diagram for U.S. Patent 7 439 409 .....	46
2.10 Virent’s BioForming Process Flow Diagram .....	50
2.11 Overview of Virent’s BioForming® Platform for the Production of Biochemicals and Biofuels .....	51
2.12 Representative APR Reactant and Product Molecules .....	52
2.13 GC Compositional Comparison (left) of Virent’s BioFormate and a Typical Petroleum Reformate Stream along with a PONA Analysis Comparison (right) .....	53
3.1 Mixed Xylene Technology .....	55
3.2 Semi Regenerative Reformer Process Flow Diagram .....	59
3.3 Continuous Catalytic Reforming Process Flow Diagram.....	60
3.4 Effect of Steam Cracker Feedstock on Aromatics Yield.....	62
3.5 Effect of Severity on BTX Yields for a Full Range Naphtha Feed .....	63
3.6 Toluene Disproportionation/Transalkylation Typical Flowsheet.....	69
3.7 <i>para</i> -Xylene Production PxMax <sup>SM</sup> Process Flow Diagram.....	71
3.8 PX-Plus™ Process Flow Diagram.....	74

3.9	Xylenes Recovery Processes.....	76
3.10	Equilibrium Concentrations for C <sub>8</sub> -Aromatic Compounds.....	78
3.11	<i>para</i> -Xylene Production via UOP Parex™/Isomar Process .....	81
3.12	Eluxyl® Process Flow Diagram .....	84
3.13	<i>para</i> -Xylene Production via Crystallization/Isomerization.....	87
3.14	Cascaded Ethylene/Propylene Refrigeration System.....	90
3.15	Single-Effect AAR Cycle .....	93
3.16	Block Flow Diagram – ExxonMobil PX Crystallization Process.....	101
3.17	Xylenes Isomerization: UOP Isomar Process .....	103
4.1	BioFormPX Cost of Production Sensitivity to Investment.....	118
4.2	BioFormPX Cost of Production Sensitivity to Hydrogen Price .....	118
4.3	<i>para</i> -Xylene Cost of Production ( <i>USGC, First Quarter 2011</i> ).....	121
4.4	<i>para</i> -Xylene Cost of Production Sensitivity to Price of Bio Feed.....	122
4.5	Bio <i>para</i> -Xylene Cost of Production Sensitivity to Regional Pricing.....	123
4.6	Bio <i>para</i> -Xylene Cost of Production Sensitivity to Economy of Scale.....	124
4.7	Bio <i>para</i> -Xylene Cost of Production Sensitivity to Investment .....	125
4.8	Bio <i>para</i> -Xylene Cost of Production plus ROCE.....	126
4.9	Renewable versus Conventional Routes to PX.....	128
5.1	Global <i>para</i> -Xylene End-Use Pattern, 2010.....	131
5.2	Global <i>para</i> -Xylene Capacity, 2010.....	132
5.3	Global <i>para</i> -Xylene Net Trade .....	133
5.4	United States <i>para</i> -Xylene End-Use Pattern, 2010 .....	134
5.5	United States <i>para</i> -Xylene Supply, Demand, and Trade.....	136
5.6	Western Europe <i>para</i> -Xylene End-Use Pattern, 2010.....	137
5.7	Western Europe <i>para</i> -Xylene Supply, Demand, and Trade .....	140
5.8	Asia Pacific <i>para</i> -Xylene End-Use Pattern, 2010 .....	142
5.9	Asia Pacific <i>para</i> -Xylene Supply, Demand, and Trade.....	148

Table	Page
1.1 Isobutylene to Isooctane Process Comparison Overview.....	3
1.2 Xylene Demand versus Production.....	9
1.3 Licensors of Aromatics Technology.....	9
2.1 Isobutylene to Isooctane Process Comparison Overview.....	18
2.2 InAlk™ Oligomerization Catalyst Comparison.....	19
2.3 Dehydrocyclization Patent Search Results.....	25
2.4 Material Balance Based on Gevo's U.S. Patent Application 2011/0087000.....	37
2.5 Theoretical Feedstock Consumption for In-situ and Ex-situ Process Platforms.....	54
3.1 Xylene Demand versus Production.....	56
3.2 Licensors of Aromatics Technology.....	56
3.3 Typical Composition of Mixed Xylenes.....	57
3.4 Pyrolysis Gasoline Analysis.....	64
3.5 Reactor Operating Conditions of MSTDP and PxMax <sup>SM</sup> .....	72
3.6 C <sub>8</sub> Aromatics - Physical Properties.....	85
3.7 Typical <i>para</i> -Xylene Specification.....	105
4.1 Feedstock, Byproduct, and Utility Prices.....	107
4.2 Cost of Production Estimate for: BTX Process: Catalytic Fast Process (CFP).....	110
4.3 Cost of Production Estimate for: <i>para</i> -Xylene Process: CFP/Adsorption/Isomerization.....	111
4.4 Cost of Production Estimate for: Isobutanol Process: Gevo Corn Fermentation.....	113
4.5 Cost of Production Estimate for: <i>para</i> -Xylene Process: Fermentation followed by Isobutanol Dehydration, Dimerization, Aromatization (with Recycle of Isooctene and Isobutylene) and Recovery.....	114
4.6 Cost of Production Estimate for: BioFormPX ( <i>para</i> -Xylene) Process: BioForming (Using in-situ Hydrogen), Adsorption/Isomerization, TDP, TA.....	116
4.7 Cost of Production Estimate for: BioFormPX ( <i>para</i> -Xylene) Process: BioForming (Employing ex-situ Hydrogen), Adsorption/Isomerization, TDP, TA.....	117
4.8 Cost of Production Estimate for: <i>para</i> -Xylene Process: Naphtha Hydrotreating, Reforming, Adsorption/EB Isomerization, TDP, TA.....	120
5.1 Global <i>para</i> -Xylene Supply, Demand, and Trade.....	133
5.2 United States <i>para</i> -Xylene Capacity.....	135
5.3 United States <i>para</i> -Xylene Supply, Demand, and Trade.....	136
5.4 Western Europe <i>para</i> -Xylene Capacity.....	138

---

5.5	Western Europe <i>para</i> -Xylene Supply, Demand, and Trade .....	139
5.6	Asia Pacific <i>para</i> -Xylene Capacity .....	145
5.7	Asia Pacific <i>para</i> -Xylene Supply, Demand, and Trade.....	147

# CHEMSYSTEMS

## PERP PROGRAM



[www.chemsystems.com](http://www.chemsystems.com)

The ChemSystems Process Evaluation/Research Planning (PERP) program is recognized globally as the industry standard source for information relevant to the chemical process and refining industries. PERP reports are available as a subscription program or on a single report basis.

### Contact Details:

**London:** Dr. Alexander Coker, Manager, PERP Program  
Phone: + 44-(20)-7950-1570, e-mail: [acoker@nexant.com](mailto:acoker@nexant.com)

**New York:** Heidi Junker Coleman, Multi-Client Programs Administrator  
Phone: + 1-914-609-0381, e-mail: [hcoleman@nexant.com](mailto:hcoleman@nexant.com)

**Shanghai:** Dr. Y. Larry Song, General Manager, Nexant China  
Phone: +86 21 6182 6791, e-mail: [ylsong@nexant.com](mailto:ylsong@nexant.com)

Nexant, Inc. ([www.nexant.com](http://www.nexant.com)) is a leading management consultancy to the global energy, chemical, and related industries. For over 38 years, ChemSystems has helped clients increase business value through assistance in all aspects of business strategy, including business intelligence, project feasibility and implementation, operational improvement, portfolio planning, and growth through M&A activities. Nexant has its main offices in San Francisco (California), White Plains (New York), and London (UK), and satellite offices worldwide.

Copyright © by Nexant Inc. 2012. All Rights Reserved.